fraction and a high boiling fraction, and hydroisomerising the high boiling fraction into a low boiling fraction and blending the low boiling fraction and the hydroisomerised high boiling fraction to produce the additive having >90 wt% C_{16} to C_{20} paraffins of which >50 wt% are isoparaffins. This disclosure does not disclose that a diesel fuel having good cold flow properties and high cetane number can be produced, only an additive, also the disclosure requires hydroisomerisation of a high boiling fraction which leads to a loss of material from the diesel boiling range into lighter material and to the formation of branched isomers, which leads to Cetane ratings less than the corresponding n-paraffins. The disclosure also does not address the issue of cold flow properties simulataneously with high a Cetane number.

Ent A1

Also on page 2 of the international application, please insert the following paragraph at line 16:

A2

The synthetic middle distillate cut may include more than 50 mass% paraffins lighter than C_{16}.

On page 11 of the international application, please insert a line space between paragraphs 2 and 3 as indicated below:

A3

The combination of highly linear paraffins derived from the <270°C fraction and mainly branched paraffins derived from the >270°C fraction results in a superb diesel.

Important parameters for a FT work-up process are maximization of product yield, product quality and cost. While the proposed process scheme is simple and therefore cost-effective, it produces High Performance Diesel, having a Cetane number >70, and naphtha in good yield. In fact, the process of this invention is able to produce a diesel of hitherto unmatched quality, which is characterized by a unique combination of both high Cetane number and excellent cold flow properties. This is believed to be related to a low degree of isomerisation in the 160-270°C fraction of the diesel and contrary to this, a high degree of isomerisation in the 270-370°C fraction of the diesel.